THERMAL AND FLUID ANALYSIS ON EFFECTS OF A NANOFLUID OUTSIDE OF A STRETCHING CYLINDER WITH MAGNETIC FIELD USING THE DIFFERENTIAL QUADRATURE METHOD

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In this paper, magnetohydrodynamic flow (MHD) of a nonofluid over a stretching cylinder is investigated numerically. The Differential Quadrature Method (DQM) is applied for solving the governing equations. The influence of relevant parameters such as the magnetic parameter, the solid volume fraction of nanoparticles and the type of nanofluid on the flow, heat transfer, Nusselt number and skin friction coefficient is discussed. Also, comparison with the published results is presented. The results show that the Nusselt number increases with growth in the volume fraction coefficient and Reynolds number but decreases with the magnetic parameter.

Keywords: nanofluids, Differential Quadrature Method (DQM), heat transfer, streching cylinder, magnetic field

1. Introduction

Magnetohydrodynamics can be regarded as a combination of fluid mechanics and electromagnetism, that is, behaviour of an electrically conducting fluid in the presence of magnetic and electric fields. The study of magnetohydrodynamic (MHD) flow has received a great deal of research interest due to its importance in many engineering applications such as plasma studies, MHD power generators, petroleum industries, cooling of nuclear reactors, boundary layer control in aerodynamics and crystal growth (Harada and Tsunoda, 1998; Shang, 2001).

Many investigations have been done on the flow past a moving flat plate or a stretching sheet in the presence of a transverse magnetic field, and a good amount of literature has been generated on this problem (Ishak *et al.*, 2006; Mahapatra and Gupta, 2001).

Examples of such technological applications are hot rolling, wire drawing, glass-fibre and paper production, drawing of plastic films, metal and polymer extrusion and metal spinning (Magyari and Keller, 1999). In all these cases, a study of the flow field and heat transfer can be of significant importance since the quality of the final product depends to a large extent on the skin friction coefficient and the surface heat transfer rate. The heat removal strategies in many engineering applications such as cooling of electronic components rely on natural convection heat transfer due to its simplicity, minimum cost, low noise, smaller size and reliability. In most natural convection studies, the base fluid has a low thermal conductivity, which limits the heat transfer enhancement. However, the continuing miniaturization of electronic devices requires further heat transfer improvements from the energy saving viewpoint (Aminossadati and Ghasemi, 2009). An innovative technique which uses a mixture of nanoparticles and the base

fluid was first introduced by Choi (1995) in order to develop advanced heat transfer fluids with substantially higher conductivities. The resulting mixture of the base fluid and nanoparticles having unique physical and chemical properties is referred to as a nanofluid. It is expected that the presence of nanoparticles in the nanofluid will increase the thermal conductivity and, therefore, substantially enhance the heat transfer characteristics of the nanofluid. Convectional heat transfer fluids, including oil, water, and ethylene glycol mixture are poor heat transfer fluids, since the thermal conductivity of these fluids plays an important role in determining the coefficient of heat transfer between the heat transfer medium and the heat transfer surface (Ho *et al.*, 2008).

Mathematical modelling is a vantage point to reach a solution in an engineering problem, so the accurate modelling of nonlinear engineering problems is an important step to obtain accurate solutions (Zolfagharian *et al.*, 2014a,b,c, 2015; Misagh *et al.*, 2014).

Most differential equations of engineering problems do not have exact analytical solutions, so approximation and numerical methods must be used. Recently, some different methods have been introduced to solving these equations, such as the Variational Iteration Method (VIM) (Ghasemi et al., 2012), Homotopy Perturbation Method (HPM) (Ghasemi et al., 2013; Mohammadian et al., 2015), Parameterized Perturbation Method (PPM) (Ghasemi et al., 2015c), Differential Transformation Method (DTM) (Ghasemi et al., 2014a,c; Hatami et al., 2015), Homotopy Analysis Method (HAM) (Ziabakhsh and Domairry, 2009; Ziabakhsh et al., 2010), Adomian Decomposition Method (Ghasemi et al., 2012), Modified Homotopy Perturbation Method (MHPM) (Ghasemi et al., 2014d), Least Square Method (LSM) (Ghasemi et al., 2014c, 2015b; Darzi et al., 2015), Collocation Method (CM) (Ghasemi et al., 2015a; Atouei et al., 2015), Galerkin Method (GM) (Ghasemi et al., 2015d), and Optimal Homotopy Asymptotic Method (OHAM) (Vatani et al., 2014; Valipour et al., 2015). Also, the Differential Quadrature Method (DQM) is a numerical technique for solving differential equations. It was first developed by Bellman et al. (1972). Afterwards, it was improved by Shu (2000). The magnetohydrodynamic natural convection boundary-layer flow on a sphere in a porous medium was studied numerically using the Differential Quadrature Method (DQM) by Moghimi et al. (2011). The boundary-layer natural convection flow on a permeable vertical plate with thermal radiation and mass transfer was investigated when the plate moved in its own plane by Talebizadeh et al. (2011). They solved the governing equations by means of an excellent analytical method called Homotopy Analysis Method (HAM) and a higher-order numerical method, namely the Differential Quadrature Method (DQM). Hatami and Ganji (2014) applied the Differential Transformation Method with the Padé approximation (DTM-Padé) and the Differential Quadrature Method (DQM) for the motion of a particle in a forced vortex. They showed that the results of the DQM were in excellent agreement with the numerical forth-order Runge-Kutta solution.

Ghasemi *et al.* (2016a) applied the Differential Quadrature Method (DQM) to find an accurate solution for blood flow analysis in femoral and coronary arteries. They showed that the results of the DQM were in excellent agreement with the numerical Crank Nicholson Method (CNM).

Application of the Differential Quadrature Method (DQM) for boundary layer flow over a flat plate with slip flow and constant heat flux surface condition was studied by Moghimi *et al.* (2013). Wang (1988) studied the steady flow of a viscous and incompressible fluid outside of a stretching hollow cylinder in an ambient fluid at rest. Ishak *et al.* (2008) investigated the flow and heat transfer of a viscous and incompressible electrically conducting fluid outside of a stretching cylinder in the presence of a constant transverse magnetic field. The problem is governed by a third-order nonlinear ordinary differential equation that leads to exact similarity solutions of the Navier-Stokes equations.

The main aim of this paper is to simulate the problem of the flow of a nanofluid outside of a stretching cylinder in the presence of magnetic field by DQM and to compare the obtained results with those of Ishak *et al.* (2008), which represent the influence of adding nanoparticles to the base fluid. Also, the effects of some parameters such as the solid volume fraction of nanoparticles, type of the nanofluid and the magnetic parameter on velocity and temperature profiles are examined.

2. Formulation of the problem

Consider a steady laminar flow of an incompressible electrically conducting fluid (with electrical conductivity σ) caused by a stretching tube of radius a in the axial direction in the fluid at rest as shown in Fig. 1, where the z-axis is measured along the axis of the tube and the r-axis is measured in the radial direction. It is assumed that the surface of the tube is at constant



Fig. 1. Physical model and coordinate system

temperature T_w and the ambient fluid temperature is T_1 , where $T_w > T_1$. We also assume that the uniform magnetic field of intensity B_0 acts in the radial direction and that the effect of the induced magnetic field is negligible, which is valid when the magnetic Reynolds number is small. The viscous dissipation, Ohmic heating and Hall effects are neglected as they are also assumed to be small. The fluid is a water based nanofluid containing different types of nanoparticles: Cu, Al₂O₃ and TiO₂. It is assumed that the base fluid and the nanoparticles are in thermal equilibrium and no slip occurs between them. The thermo physical properties of the nanofluid are given in Table 1

Table 1	. Thermo-physical	properties of	water and	nanoparticles ((Oztop and A)	Abu-Nada, 2008)
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	$ ho [kg/m^3]$	$C_p [\mathrm{J/(kgK)}]$	k [W/(mK)]	$\beta [1/K]$
Pure water	997.1	4179	0.613	21
Copper (Cu)	8933	385	401	1.67
Silver (Ag)	10500	235	429	1.89
Alumina (Al_2O_3)	3970	765	40	0.85
Titanium Oxide (TiO_2)	4250	686.2	8.9538	0.9

(see Oztop and Abu-Nada, 2008). On the above assumptions, the boundary layer equations governing the flow, and the concentration field can be written in dimensional form as

$$\frac{\partial(ru)}{\partial r} + \frac{\partial(rw)}{\partial z} = 0 \qquad u\frac{\partial w}{\partial r} + w\frac{\partial w}{\partial z} = \frac{\mu_{nf}}{\rho_{nf}} \left(\frac{\partial^2 w}{\partial r^2} + \frac{1}{r}\frac{\partial w}{\partial r}\right) - \frac{\sigma B_0^2}{\rho_{nf}}w$$

$$u\frac{\partial u}{\partial r} + w\frac{\partial u}{\partial z} = -\frac{1}{\rho_{nf}}\frac{\partial p}{\partial r} + \frac{\mu_{nf}}{\rho_{nf}} \left(\frac{\partial^2 u}{\partial r^2} + \frac{1}{r}\frac{\partial u}{\partial r} - \frac{u}{r^2}\right)$$

$$(\rho C_p)_{nf} \left(w\frac{\partial T}{\partial z} + u\frac{\partial T}{\partial r}\right) = k_{nf} \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r}\frac{\partial T}{\partial r}\right)$$
(2.1)

Subject to the following boundary conditions

$$u = 0 w = W_w T = T_w at r = a w \to 0 T \to T_\infty as r \to \infty (2.2)$$

where u and w are the velocity components along the r and z axes, respectively, $W_w = 2cz$ where c is a positive constant, and a is a constant. Further, ν , ρ , T and α are the kinematic viscosity, fluid density, fluid temperature and thermal diffusivity, respectively. It is necessary to mention that the magnetic term in Eq. (2.1)₃ (in the r direction) is neglected because it does not affect the flow dynamics in perpendicular situations and can be absorbed by the pressure term.

The effective density ρ_{nf} , the effective dynamic viscosity μ_{nf} , the heat capacitance $(\rho Cp)_{nf}$ and the thermal conductivity k_{nf} of the nanofluid are given as (see Aminossadati and Ghasemi, 2009)

$$(\rho C_p)_{nf} = (\rho C_p)_f (1 - \varphi) + (\rho C_p)_s \varphi \qquad \qquad \frac{k_{nf}}{k_f} = \frac{k_s + 2k_f - 2\varphi(k_f - k_s)}{k_s + 2k_f + \varphi(k_f - k_s)}$$

$$\rho_{nf} = \rho_f (1 - \varphi) + \rho_s \varphi \qquad \qquad \mu_{nf} = \frac{\mu_f}{(1 - \varphi)^{2.5}}$$

$$(2.3)$$

Here, φ is the solid volume fraction, μ_f is the dynamic viscosity of the basic fluid, ρ_f and ρ_s are the densities of the pure fluid and nanoparticle, respectively. $(\rho C_p)_f$ and $(\rho C_p)_s$ are the specific heat parameters of the base fluid and nanoparticle, k_f and k_s are the thermal conductivities of the base fluid and nanoparticle, respectively. Following Wang (1988), we take the similarity transformation

$$u = -ca\frac{f(\eta)}{\sqrt{\eta}} \qquad \qquad w = 2cf'(\eta)z \qquad \qquad \eta = \left(\frac{r}{a}\right)^2 \qquad \qquad \theta = \frac{T - T_{\infty}}{T_w - T_{\infty}} \tag{2.4}$$

where the prime denotes differentiation with respect to η . Substituting Eq. (14) into Eqs. (2.1)₂ and (2.1)₄, we get the following ordinary differential equations

$$\frac{1}{(1-\varphi)^{2.5}} \frac{1}{1-\varphi + \frac{\rho_s}{\rho_f}\varphi} (f'''\eta + f'') - \frac{M}{1-\varphi + \frac{\rho_s}{\rho_f}\varphi} f' - \operatorname{Re} f'^2 + \operatorname{Re} f f'' = 0$$

$$\theta''\eta + \theta' + f\theta' \operatorname{Re} \operatorname{Pr} \frac{1-\varphi + \frac{(\rho C_p)_s}{(\rho C_p)_f}\varphi}{\frac{k_s + 2k_f - 2\varphi(k_f - k_s)}{k_s + 2k_f + \varphi(k_f - k_s)}} = 0$$
(2.5)

where Re = $ca^2/(2\nu_{nf})$ is the Reynolds number and $M = \sigma B_0^2 a^2/(4\nu_{nf}\rho_{nf})$ is the magnetic parameter. ν_{nf} is the kinematic viscosity of nanofluid. Boundary conditions (2.2) become

$$f(1) = 0 \qquad f'(1) = 1 \qquad \theta(1) = 1$$

$$f(\infty) \to 0 \qquad \theta(\infty) \to 0 \qquad (2.6)$$

The pressure can now be determined from Eq. $(2.1)_3$ in the following form

$$\frac{p - p_{\infty}}{\rho cv} = -\frac{\operatorname{Re}}{\eta} f^2(\eta) - 2f'(\eta)$$
(2.7)

The physical quantities of interest are the skin friction coefficient and the Nusselt number, which are defined as follows

$$C_f = \frac{\tau_w}{\rho W_w/2} \qquad \qquad \text{Nu} = \frac{aq_w}{k(T_w - T_\infty)} \tag{2.8}$$

Furthermore, τ_w and q_w are the skin friction and the heat transfer from the surface of the tube, respectively, and are given as

$$\tau_w = \mu \left(\frac{\partial w}{\partial r}\right)_{r=a} \qquad q_w = -k \left(\frac{\partial T}{\partial r}\right)_{r=a} \tag{2.9}$$

where k is the thermal conductivity. Considering variables (2.4), we get

$$C_f \frac{\text{Re}z}{a} = f''(1)$$
 $\text{Nu} = -2\theta'(1)$ (2.10)

3. Differential Quadrature Method (DQM)

The differential quadrature method (DQM) is a rather efficient numerical method for rapid solution of linear and nonlinear partial differential equations (Bellman *et al.*, 1972). Compared with the conventional methods such as the finite element and finite difference methods, the DQM requires less computer time and storage.

In this study, a polynomial expansion based differential quadrature, as introduced by Quan and Chang (1989), is applied for solving the problem. Several attempts have been made by researchers to develop polynomial based differential quadrature methods. One of the most useful approaches is the one that uses the following Lagrange interpolation polynomials as test functions

$$g_k = \frac{M(x)}{(x - x_k)M^{(1)}(x_k)} \qquad k = 1, 2, \dots, N$$
(3.1)

where

$$M(x) = (x - x_1)(x - x_2) \cdots (x - x_N) \qquad M^{(1)}(x_i) = \prod_{\substack{k=1\\k \neq i}}^N (x_i - x_k)$$
(3.2)

By applying the above equation at N grid points, the following algebraic formulations to compute the weighting coefficients are developed

$$A_{ij}^{(1)} = \frac{1}{x_j - x_i} \prod_{\substack{k=1\\k \neq i,j}}^{N} \frac{x_i - x_k}{x_j - x_k} \qquad i \neg j$$

$$A_{ij}^{(1)} = \sum_{\substack{k=1\\k \neq i}}^{N} \frac{1}{x_i - x_k} \qquad A_{ij}^{(2)} = \sum_{k=1}^{N} A_{ik}^{(1)} A_{kj}^{(1)} \qquad (3.3)$$

where $A^{(1)}$ and $A^{(2)}$ denote the weighting coefficients of the first and second order derivatives of the function f(r) with respect to the r direction. N is the number of grid points chosen in the r direction. The differential quadrature approximation can be easily extended from the above formulation to other coordinates. The first order derivatives in the two-dimensional formulation are approximated by

$$\frac{\partial f}{\partial r}\Big|_{ij} \approx \sum_{l=1}^{N} A_{il}^{(1)} f_{lj} \qquad \frac{\partial f}{\partial z}\Big|_{ij} \approx \sum_{m=1}^{M} B_{jm}^{(1)} f_{im}$$
(3.4)

And the second order derivatives can be approximated by:

$$\frac{\partial f}{\partial r}\Big|_{ij} \approx \sum_{l=1}^{N} A_{il} f_{lj} \qquad \frac{\partial^2 f}{\partial r^2}\Big|_{ij} \approx \sum_{l=1}^{N} A_{il}^{(2)} f_{lj}
\frac{\partial f}{\partial z}\Big|_{ij} \approx \sum_{m=1}^{P} B_{jm} f_{im} \qquad \frac{\partial^2 f}{\partial z^2}\Big|_{ij} \approx \sum_{n=1}^{P} B_{kn}^{(2)} f_{ijn}
\frac{\partial^2 f}{\partial r \partial z}\Big|_{ij} \approx \sum_{l=1}^{N} A_{il}^{(1)} \sum_{m=1}^{P} B_{jm}^{(1)} f_{lm}$$
(3.5)

where $A^{(1)}$ and $B^{(1)}$ denote the weighting coefficients of the first order derivatives; $A^{(2)}$ and $B^{(2)}$ denote the weighting coefficients of the second order derivatives of the function f(r, z) with respect to the r and z-directions, respectively; N and P are the number of grid points chosen in the r and z-directions, respectively.

4. Results and discussion

Equations (2.5) along with their boundary conditions are solved numerically by using the DQM. After applying this method, the influence of several non-dimensional parameters, namely the Reynolds number Re, Prandtl number Pr, nanoparticles volume fraction φ and magnetic parameter M, have been investigated. Validating the numerical results obtained in this study, the case when the volume fraction coefficient is zero ($\varphi = 0$) has been considered and compared with the previously published results in Tables 2 and 3. These tables present numerical values of the skin friction coefficient in terms of f''(1) and the Nusselt number Nu in terms of $-\theta'(1)$ along with the results reported by Ishak *et al.* (2008), which show an excellent agreement with the achieved results in the present study.

М	Re = 1		Re = 5		
11/1	Present work	Ishak $et al. (2008)$	Present work	Ishak <i>et al.</i> (2008)	
0	-1.17849	-1.1780	-2.41745	-2.4174	
0.01	-1.18431	-1.1839	-2.41990	-2.4199	
0.05	-1.20708	-1.2068	-2.42965	-2.4296	
0.10	-1.23454	-1.2344	-2.44174	-2.4417	
0.50	-1.42693	-1.4269	-2.53523	-2.5352	

Table 2. Values of the skin friction coefficient for several values of M and Re at Pr = 6.2

Table 3. Values of the Nusselt number for several values of M and Re at Pr = 6.2

М	Re = 1		Re = 5		
	Present work	Ishak $et al. (2008)$	Present work	Ishak <i>et al.</i> (2008)	
0	2.05857	2.0587	19.1185	19.1587	
0.01	2.05715	2.0572	19.1184	19.1586	
0.05	2.05158	2.0516	19.1179	19.1581	
0.10	2.04487	2.0449	19.1174	19.1576	
0.50	1.99806	1.9978	19.1129	19.1530	

Figure 2 shows the effect of volume fraction coefficient φ on velocity distribution for Re = 5. It is noticed that the Prandtl number Pr gives no effect to the velocity as can be seen from Eq. $(2.5)_1$. The velocity curves show that the rate of transport is considerably reduced with an increase of φ . In all cases, the velocity vanishes at some large distance from the surface of the tube.



Fig. 2. Velocity profiles for various values of φ (Re = 5, M = 5, Pr = 6.2)

Figure 3 presents temperature profiles for various values of φ when $\Pr = 6.2$ and $\operatorname{Re} = 5$, and the nanoparticle is Cupper. It is obvious that the temperature increases as φ increases, but it decreases as the distance from the surface increases, and finally vanishes at a some large distance from the surface. Consider that $\varphi = 0$ represents pure water like what is presented by Ishak *et al.* (2008). It is clear that the heat transfer in the present case is more than the case when the fluid is pure water.



Fig. 3. Temperature profiles for various values of φ (Re = 5, M = 5, Pr = 6.2)

Figure 4a exhibits the skin friction coefficient profiles C_f for various values of the Reynolds number Re as M is constant. It is observed that the magnitude of the skin friction coefficient increases as Re increases. Figure 4b represents the skin friction coefficient profiles C_f for various values of M when the Reynolds number Re is constant. It can be seen that the magnitude of the skin friction coefficient grows as M increases.

Furthermore, it is clear from both Figs. 4a,b that the skin friction coefficient increases with an increase in the volume fraction coefficient. The same behavior can be observed for the Nusselt number, i.e. growing Re increases the temperature gradient and, in turn, increases the Nusselt number. And an increase in M decreases the Nusselt number, which is obvious from Figs. 5a,b. Also, it is clear that the Nusselt number increases with an increase in the volume friction coefficient.

After the velocity $f'(\eta)$ is obtained, the pressure p in terms of $(p - p_{\infty})/(\rho cv)$ can be found by using Eq. (2.7). The numerical results are shown in Fig. 6a for M = 2, $\varphi = 0.1$ and Re = 1, 5



Fig. 4. Skin friction coefficient for various values of (a) Re and φ (M = 2, Pr = 6.2), (b) M and φ (Re = 5, Pr = 6.2)



Fig. 5. Nusselt number for various values of (a) Re and φ (M = 2, Pr = 6.2), (b) M and φ (Re = 5, Pr = 6.2)



Fig. 6. Pressure distribution obtained from Eq. (2.7) for various values of (a) Re ($\varphi = 0.1$, M = 2, Pr = 6.2), (b) φ (Re = 10, M = 2, Pr = 6.2)

and 10. All curves show that $p \to p_{\infty}$ far away from the surface $\eta \to \infty$. Further, Fig. 6b shows the pressure curve for different values of φ when Re = 10 and M = 2. It is clear from this figure that bigger values of φ result in slower algebraic decay. In other words, if $\varphi = 0.2$, sufficient decay of $(p - p_{\infty})$ takes place at higher values of η than the case when $\varphi = 0$.

Figures 7a and 7b represent $f'(\eta)$ and $\theta(\eta)$ curves, respectively, for different types of nanoparticles, namely, Cu, Al₂O₃ and TiO₂ when $\varphi = 0.1$, M = 5, Pr = 6.2, and Re = 5. The figure shows that by using different types of nanofluids, values of the velocity and temperature change, i.e. we can say that the sheer stress and the rate of hate transfer change by using different types of nanofluids. This means that the nanofluids will be important in the cooling and heating processes.



Fig. 7. (a) Velocity profiles and (b) temperature profiles for various values of nonoparticles ($\varphi = 0.1$, Re = 5, M = 5, Pr = 6.2)

5. Conclusions

A steady two dimensional flow of an electrically conducting incompressible nanofluid due to stretching cylindrical tube is studied in the present work. Similarity solutions are obtained for a linearly stretching tube with a constant surface temperature, and the achieved ordinary differential equations are solved numerically by applying the Differential Quadrature Method (DQM). Effects of the volume fraction coefficient, magnetic parameter and Reynolds number on the flow and heat transfer characteristics have been examined. It can be concluded that the magnitude of the skin friction coefficient increases with the volume fraction coefficient, magnetic parameter and Reynolds number, while it is constant with the Prandtl number. The Nusselt number, also, increases with the volume fraction coefficient and Reynolds number but decreases with the magnetic parameter.

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